

IN THE CLAIMS:

Please cancel Claims 23-25:

13. (Previously Presented) A process for producing spherical nickel hydroxide comprising:

(a) subjecting a nickel electrode to anodic dissolution in a completely intermixed electrolysis cell and using an electrolysis brine that is introduced into the cell and that has (i) a chlorine ion content ranging from 20 to 50 g/l (ii) an ammonia content ranging from 1 to 7 g/l of (iii) a pH value ranging from 9.5 to 11.5 and (iv) a temperature of 45 to 60°C; and

(b) precipitating nickel hydroxide.

14. (Previously Presented) The process according to Claim 13, wherein before introducing the electrolysis brine into the electrolysis cell, the pH of the electrolysis brine is adjusted to a value ranging from 10 to 10.5 by addition of alkali metal hydroxide or hydrochloric acid to the brine.

15. (Previously Presented) The process according to Claim 13, wherein the brine has a circulation rate that is at least 20 cm/s.

16. (Previously Presented) The process according to Claim 13, wherein the molar ratio of chloride ions to ammonia is from 2 to 10.

17. (Previously Presented) The process according to Claim 13, wherein the electrolysis brine has an average residence time ranging from 1 to 5 hours.

18. (Previously Presented) The process according to Claim 13 further comprising continuously introducing into the electrolysis cell a doping metal ion selected from the group consisting of Co, Zn, Mg, Cu, Cr, Fe, Sc, Y, La, lanthanoids, B, Ga, Mn, Cd and Al.

19. (Previously Presented) The process according to Claim 18, wherein the doping element ions are produced by anodic oxidation of the corresponding metals.

20. (Previously Presented) The process according to Claim 13 further comprising discharging brine containing dispersed nickel hydroxide powder from the electrolysis cell, separating nickel hydroxide powder and returning the brine to the electrolysis cell.

21. (Previously Presented) The process according to Claim 13 further comprising discharging brine containing dispersed nickel hydroxide powder from the

Mo-6747

electrolysis cell and introducing the brine containing dispersed nickel hydroxide into a downstream electrolysis cell having a metallic cobalt anode.

22. (Previously Presented) The process according to Claim 21 further comprising discharging brine containing nickel hydroxide powder coated with cobalt hydroxide from the electrolysis cell containing metallic cobalt, separating the nickel hydroxide powder and returning the brine to the electrolysis cell.

23 - 25. (Cancelled)